



# Mathematical Study of Generalized Chemically Reactive NonNewtonain (Eyring-Powell) Material Capturing Varying Thermal Aspect Developing Cattaneo-Christov Concept

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## Abstract

This study investigates the effects of a nonlinear stretched surface in a two-dimensional Modified Eyring-Powell liquid due to a double stratified chemical reactive flow of non-Fourier heat flux. We study the flux model which is the generalized form of Fourier's classical expression with thermal relaxation time. The temperature-dependent thermal conductivity is taken into consideration and the stretched surface's thickness is variable. The similarity transformation approach is used to convert the governing system of PDEs into a collection of connected nonlinear ordinary differential systems. The resulting problems are tackled via the application of homotopy analysis approach. Skin friction coefficient, Sherwood number, temperature, concentration,

and non-dimensional velocity are all visually presented and thoroughly examined.

**Keywords:** variable sheet thickness, non-linear stretching sheet, non-Fourier heat flux, modified eyring powell liquid, variable thermal conductivity.

## 1 Introduction

The analysis of extended flows involving chemical reactions is crucial in many branches of research and engineering. The effects of heat and mass transfer in flow cannot be disregarded, especially when building equipment for food processing, freezing crops, producing and dispersing fog, and chemical processing. Furthermore, a wide range of industrial and engineering applications, including metallurgy, combustion systems, solar collectors, chemical engineering, and nuclear reactor safety, rely



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on the efficiency of this kind of flow. Chemical reactions' impact was a common feature in study reports written by researchers. When a viscous liquid flows through a permeable channel, for instance, Srinivas studies the chemically reactive flow of the liquid [1]. Zhang et al. [2] examines how heat radiation and chemical reactions affect nanofluid flow through porous material that is saturating it. When chemical processes and transpiration were present, Mabood et al. [3] investigated the MHD flow of a viscous liquid. Casson liquid's chemically reactive flow towards a vertical cone is studied by Mythili and Sivaraj [4]. For a chemically reactive two-phase magneto nanomaterial, Eid [5] proposes an exponentially stretched surface analysis. Thermophoresis, nonlinear thermal radiation, and chemically reactive bioconvective flow of magneto nanomaterial towards the upper horizontal surface of a rotating paraboloid were investigated by Makinde and Animasaun [6].

Numerous technical and industrial processes involve the transport of heat. Some particular examples of these processes are energy production, space cooling, copper material production, heat conduction in tissues, nuclear reactor cooling, and so on. Many researchers have employed baron de Fourier's law [7] of heat conduction, one of the most useful models in continuous mechanics, to improve our understanding of the characteristics of heat transmission. This law has the drawback of producing a parabolic energy equation, which shows how the initial disturbance quickly affects the entire system. Cattaneo [8] used thermal relaxation time to modify traditional Fourier's law in order to control this restriction. By utilizing Oldroyd's upper-convected derivatives to propose a frame-indifferent generalization, Christov [9] enhanced Cattaneo [9]'s approach. In this area, numerous investigations have been conducted since Christov's [9] groundbreaking work. The heat transport model proposed by Cattaneo [8] and Christov [9] for thermal convection in viscous materials was examined by Straughan [10].

The non-Newtonian materials include blood, drilling mud, printer ink, soup, butter, cheese, ketchup, jam, mayonnaise, and hydrogenated colloidal suspension. Powell and Eyring were introduced to the Eyring-Powell fluid model in 1944. The empirical representation of its constitutive link and its Newtonian behavior at both high and low shear rates distinguish this particular model. The sources provide studies that back up the Eyring-Powell fluid

model [11–13]. However, a detailed examination of the previously described works reveals that Eyring-Powell is also capable of exhibiting fluid properties that thicken under shear. This explains the discrepancies in the data on the impact of the material characteristic on flow velocity. Analysis of the modified Fourier law for the ferromagnetic flow Zubair et al. [14] investigates the Powell-Eyring fluid with the assumption of two equal magnetic dipoles.

The major objective of this work is to investigate a non-Fourier heat flux on a nonlinear stretched surface in which a two-dimensional Modified Eyring-Powell liquid with double stratified chemical reactive flow is demonstrated. Using a similarity transformation method, the governing expression is transformed into a set of coupled nonlinear ordinary differential systems. Homotopy analysis is used to solve the resulting problems. We examine the temperature, skin friction, and velocity for several of other variables that may be mentioned in the problem statement.

## 2 Mathematical Modeling

Consider a double stratified chemical reactive flow of non-Fourier heat flux due to a nonlinear stretched surface in a two-dimensional Modified Eyring-Powell liquid. The  $x$ -axis is taken along the stretching sheet with the slit at the origin, and the  $y$ -axis is normal to the sheet. Thermal conductivity is considered to be temperature-dependent. The Non-Fourier heat flux is utilized in the method of heat transfer. Furthermore, surface is at  $y = A(x + b)^{\frac{1-n}{2}}$ . We denote the variable concentration at and away from the sheet as  $(T_\infty, C_\infty)$  and the variable temperature as  $(T_w, C_w)$ . The continuity, momentum and temperature field equations after the boundary approximations are:

$$\partial_x u + \partial_y v = 0, \quad (1)$$

$$\begin{aligned} u\partial_x u + v\partial_y u &= \frac{\mu}{\rho}\partial_{yy} u \\ &+ \frac{q}{\rho} \left( \frac{1}{BC} \right)^q \left( 1 + \frac{q+2}{6C^2} (\partial_y u)^2 \right) (\partial_y u)^{q-1} \partial_{yy} u, \end{aligned} \quad (2)$$

$$\begin{aligned} u\partial_x T + v\partial_y T + \lambda^* (u\partial_x u\partial_x T + v\partial_y u\partial_y T + v\partial_y u\partial_x T \\ + 2uv\partial_{xy} T + u^2\partial_{xx} T + v^2\partial_{yy} T) = -\frac{1}{\rho c_p} k(T) \partial_{yy} T, \end{aligned} \quad (3)$$

$$u\partial_x C + v\partial_y C = D\partial_{yy} C - K^*(C - C_\infty), \quad (4)$$

with conditions.

$$\begin{aligned} u &= U_w(x) = U_0(x + b)^n, \\ v &= 0, \\ T &= T_w = T_0 + c(x + b), \end{aligned} \quad (5)$$

$$C = C_w = C_0 + c^*(x + b) \quad \text{at} \quad y = A(x + b)^{\frac{1-n}{2}}, \quad (6)$$

$$\begin{aligned} u &\rightarrow 0, \quad T \rightarrow T_\infty = T_0 + d(x + b), \\ C &= C_w = C_0 + d^*(x + b) \quad \text{as} \quad y \rightarrow \infty. \end{aligned} \quad (7)$$

The thermal conductivity in this case is represented by the formula  $k(T) = k_\infty(1 + \epsilon_1\theta)$ , where  $k_\infty$  is the ambient fluid's thermal conductivity,  $\epsilon$  the small scalar parameter that shows how temperature affects variable thermal conductivity,  $(b, c, d, c^*, d^*)$  the dimensionless constants,  $\mu$  the coefficient of dynamic viscosity,  $\theta$  the dimensionless temperature,  $K^*$  the reaction rate and  $\rho$  the fluid density. The fluid parameters in this case are B and C, the Modified Eyring Powell fluid parameters; the specific heat is  $c_p$ ,  $T$  the temperature and  $T_\infty$  the ambient temperature, the temperature, and  $(u, v)$  are the velocity components in the  $(x, y)$  directions, and  $q$  is the deformation rate, respectively.

Using the following transformations.

$$\begin{aligned} \chi &= \sqrt{\frac{2}{n+1}U_0v(x+b)^{n+1}F(\xi)}, \\ \xi &= \sqrt{\left(\frac{n+1}{2}\right)\left(\frac{U_0}{v}\right)(x+b)^{n-1}}, \\ u &= U_0(x+b)^nF'(\xi). \end{aligned} \quad (8)$$

$$\begin{aligned} v &= -\sqrt{\left(\frac{n+1}{2}\right)U_0v(x+b)^{n-1}}\left(F(\xi) + \xi\frac{n-1}{n-1}F'(\xi)\right), \\ \theta(\xi) &= \frac{T - T_\infty}{T_w - T_\infty}, \\ \phi(\xi) &= \frac{C - C}{C_w - C_\infty} \end{aligned} \quad (9)$$

By the use of Eq. (6) into the Eqs.(2-4), we get:

$$\begin{aligned} (1 + Kq\sqrt{\frac{n+1}{2}\delta F''})^{q-1}(1 - \frac{q+2}{3}\delta(F'')^2)F''' \\ + FF'' - \frac{2n}{n+1}(F')^2 = 0. \end{aligned} \quad (10)$$

$$\begin{aligned} (1 + \epsilon_1\theta)\theta'' + \epsilon_1\theta'^2 + PrF\theta' \\ + Pr\left(\frac{n-3}{2}F\theta'F' - \frac{n+1}{2}F^2\theta''\right) \\ + Pr(S_1 + \theta)(rF'F'' - \frac{2}{n+1}F' - \frac{2n}{n+1}rF^2) = 0. \end{aligned} \quad (11)$$

$$\phi'' + ScF\phi' - \frac{2Sc}{n+1}(S_2F' + \phi F' + \lambda\phi) = 0. \quad (12)$$

with:

$$\begin{aligned} F'(\alpha) &= 1, \quad F(\alpha) = \alpha\frac{1-n}{1+n}, \\ \theta(\alpha) &= 1 - S_1, \quad \phi(\alpha) = 1 - S_2, \\ F'(\infty) &= 0, \quad \theta(\infty) = 0, \quad \phi(\infty) = 0 \end{aligned} \quad (13)$$

Now we have  $F(\xi) = f(\xi - \alpha) = f(\eta)$ ,  $\theta(\xi) = \theta(\xi - \alpha) = \theta(\eta)$  and  $\phi(\xi) = \phi(\xi - \alpha) = \phi(\eta)$  then Eq. (8-10) becomes.

$$\begin{aligned} \left(1 + Kq\sqrt{\frac{n+1}{2}\delta f''}\right)^{q-1} \left(1 - \frac{q+2}{3}\delta(f'')^2\right)f''' \\ + ff' - \frac{2n}{n+1}(f')^2 = 0. \end{aligned} \quad (14)$$

$$\begin{aligned} (1 + \epsilon_1\theta)\theta'' + \epsilon_1\theta'^2 \\ + Prf\theta' + Pr\left(\frac{n-3}{2}f\theta'f' - \frac{n+1}{2}f^2\theta''\right) \\ + Pr(S_1 + \theta)(yff'' - \frac{2}{n+1}f' - \frac{2n}{n+1}yf^2) = 0. \end{aligned} \quad (15)$$

$$\phi'' + Scf\phi' - \frac{2Sc}{n+1}(S_2F' + \phi F' + \lambda\phi) = 0. \quad (16)$$

with

$$\begin{aligned} F(0) &= 1, \quad F(0) = \alpha\frac{1-n}{1+n}, \\ \theta(0) &= 1 - S_1, \quad \phi(0) = 1 - S_2, \\ F'(\infty) &= 0, \quad \theta(\infty) = 0, \quad \phi(\infty) = 0. \end{aligned} \quad (17)$$

Here  $K(= \frac{1}{\mu B C})$  and  $\delta(= \frac{U_0^3(x+b)^{3n-1}}{2vC^2})$  are the fluid parameters, The fluid parameters  $S_1(= \frac{d}{c})$

and  $S_2(= \frac{d^*}{c^*})$ , which represent the thermal and solutal stratification parameters. The chemical reaction parameter is represented by  $\lambda(= \frac{K^*}{U_0}(x + b)^{1-n})$ . Considering that a chemical reaction is considered generative when  $\Delta > 0$  and destructive when  $\Delta < 0$ ,  $\gamma(= \lambda^* U_0(x + b)^{n-1})$  the thermal relaxation parameter,  $Sc(= \frac{v}{D})$  the schmidt number and  $Pr(= \frac{v}{a})$ .

The skin friction coefficient and sherwood number can be expressed as:

$$C_f = \frac{2\tau_w}{\rho U_w^2}, \quad Sh_x = \frac{(x + b)q_m}{D(C_w - C_0)}. \quad (18)$$

where

$$\tau_w = \mu \partial_y u + \frac{1}{BC} \partial_y u - \frac{1}{6BC^3} (\partial_y u)^3 \quad (19)$$

$$\text{and } q_w = D \partial_y C \text{ at } y = A(x + b)^{\frac{1-n}{2}}.$$

The dimensionless form is:

$$\frac{\sqrt{Re_x} C_f}{2} = \sqrt{\frac{n+1}{2} \left( 1 + K - \frac{n+1}{2} \frac{K\delta}{3} f'(0) \right)} f'(0)$$

and  $\sqrt{Re_x} Sh_x = \sqrt{\frac{n+1}{2}} \phi'(0),$  (20)

where  $Re_x = \frac{u_w(x+b)}{v}$  the local Reynolds number.

### 3 Homotopic Procedure

The convergent solutions of Eqs. (11-13) have been obtained through the use of the HAM approach, with the boundary conditions in Eq. (14). Series form is consistent with the solutions. The first approximations and operators are written as follows:

$$\begin{aligned} f_0(\eta) &= 1 - e^{-\eta}, \\ \theta_0(\eta) &= (1 - S_1)e^{-\eta}, \\ \phi_0(\eta) &= (1 - S_2)e^{-\eta}, \end{aligned} \quad (21)$$

$$L_f = f'' - f', \quad L_\theta = \theta'' - \theta', \quad L_\phi = \phi'' - \phi'. \quad (22)$$

with

$$\begin{aligned} L_f[C_1 + C_2 e^\eta + C_3 e^{-\eta}] &= 0, \\ L_\theta[C_4 e^\eta + C_5 e^{-\eta}] &= 0, \\ L_\phi[C_6 e^\eta + C_7 e^{-\eta}] &= 0. \end{aligned} \quad (23)$$

where  $C_i(i = 1 - 7)$  defines the arbitrary constants.

### 4 Homotopic Procedure

H-Curve plays a very important role in the HAM approach, it basically shows the convergence region for Eq.(10) and Eq.(11) with the use of Eq.(12). It is observed that suitable values are:  $-1.0 \leq h_f \leq -0.5$ ,  $-1.0 \leq h_\theta \leq -0.3$  and  $-1.2 \leq h_\phi \leq -0.4$ . The H-Curve is displayed in Figure 1.

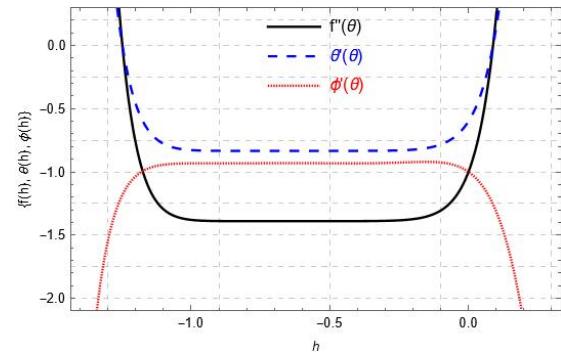


Figure 1. H-Curve for  $f''$ ,  $\theta$  and  $\phi$ .

### 5 Stability Analysis

The stability analysis for the solutions is pictured in the following Figure 2 when  $n = \delta = S_1 = 0.6$ ,  $K = \epsilon_1 = \lambda = q = 0.4$ ,  $S_2 = \gamma = \alpha = 0.1$ ,  $Sc = 0.8$  and  $Pr = 0.9$ . The graphic illustrates how the velocity gradient stabilizes at recursive step 20 and stays that way. On the other hand, the temperature gradient and concentration stabilizes at recursive step 30 and elsewhere.

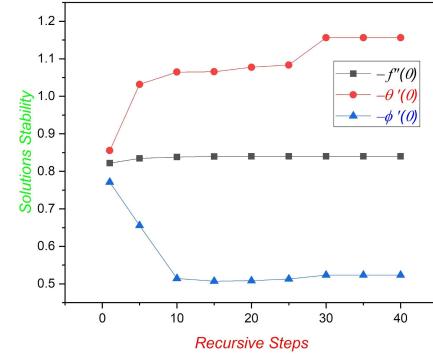
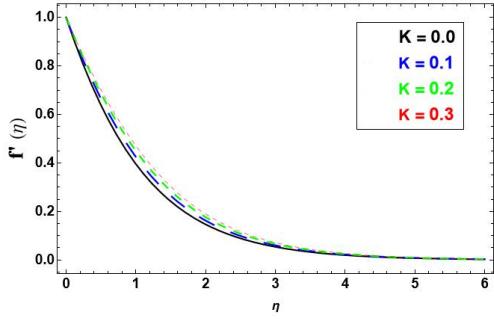
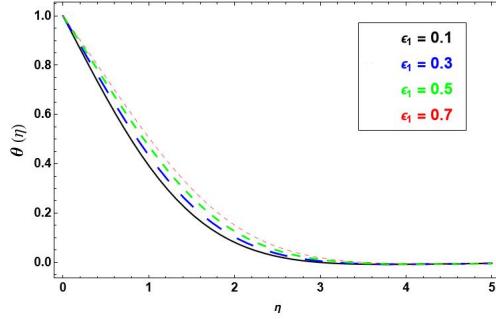
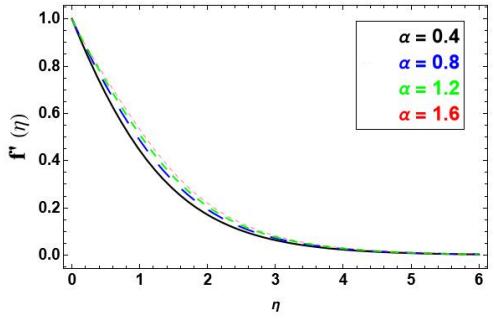
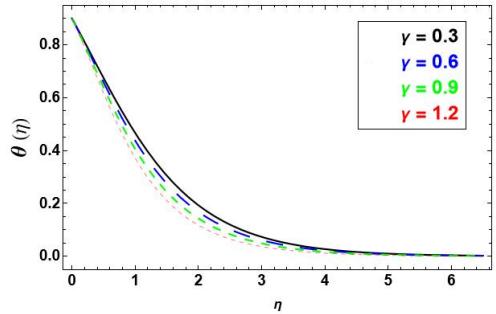
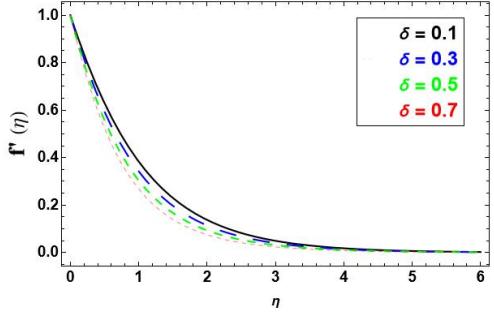
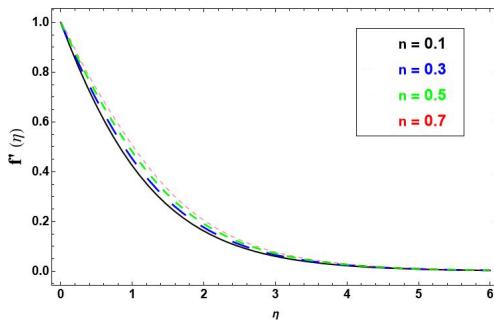


Figure 2. Stability Analysis.

### 6 Analysis

The outcomes of key variables on skin friction, temperature, and velocity are addressed in this section. To achieve this, Figures 3 to 17 are presented.

The behavior of  $K$  on  $f'$  is shown in Figure 3. It is investigated whether  $f'$  and the layer thickness

Figure 3.  $K$  via  $f'$ .Figure 7.  $ε_1$  via  $f'$ .Figure 4.  $α$  via  $f'$ .Figure 8.  $γ$  via  $f'$ .Figure 5.  $δ$  via  $f'$ .Figure 6.  $n$  via  $f'$ .

viscosity, are the effects of higher  $K$ . Figure 4 illustrates how  $α$  affects  $f'$ . The velocity and momentum layer thickness grow with increasing  $α$ . Figure 5 displays the characteristics of  $δ$  on  $f'$ . Here, the velocity and associated layer thickness show decreasing behavior for larger  $δ$ . The behavior of  $n$  on velocity  $f'$  is depicted in Figure 6. It is evident that as  $n$  increases, so does  $f'$ . Figure 7 shows the impact of  $ε_1$  on temperature  $θ$ . A larger  $ε_1$  increases the temperature  $θ$ . In terms of physical properties, thermal conductivity increases with bigger  $ε_1$  because it allows for significant heat transfer from the sheet to the substance, which raises temperature  $θ$ . The behavior of  $γ$  on temperature  $θ$  is seen in Figure 8. Here, the function of  $γ$  is decreasing with temperature  $θ$ . In addition, heat transport occurs quickly when  $γ = 0$ . The behavior of  $S_1$  at temperature  $θ$  is displayed in Figure 9. In this case, as  $S_1$  is enhanced, temperature  $θ$  and thermal layer thickness decrease. For larger  $S_1$ , the physical difference between the ambient and surface temperature  $θ$  decreases. It is corresponding to a decrease in temperature  $θ$ . The behavior of  $n$  at temperature  $θ$  is depicted in Figure 10. It is evident that temperature  $θ$  rises as  $n$  increases. Figure 11 shows the effect of  $Pr$  on temperature  $θ$ . An increase in  $Pr$  will result in a large decrease in the thermal boundary layer and temperature  $θ$ .

that corresponds to it improves. Increased velocity and momentum layer thickness, as well as decreased

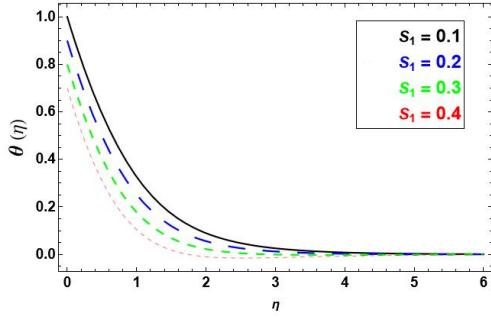
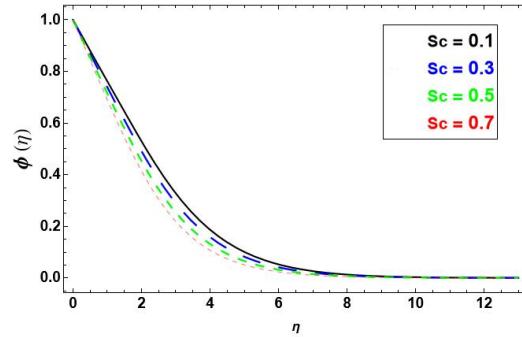
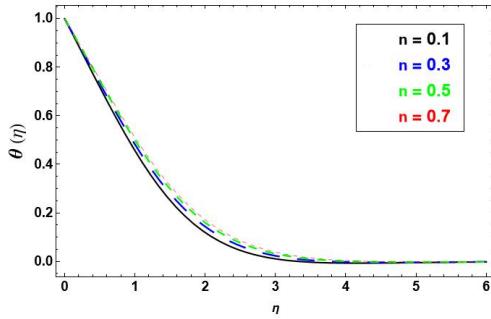
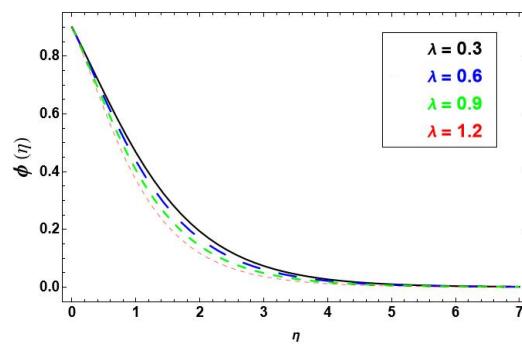
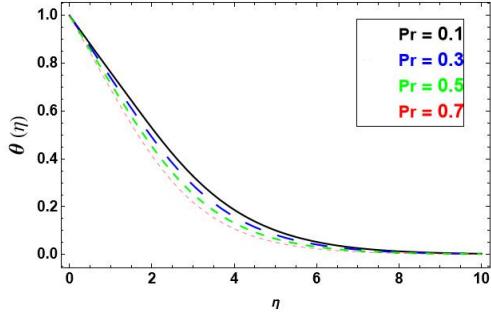
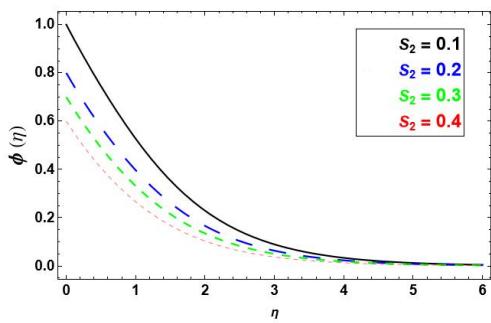
Figure 9.  $S_1$  via  $\theta$ .Figure 13.  $Sc$  via  $\phi$ .Figure 10.  $n$  via  $\theta$ .Figure 14.  $\lambda$  via  $\phi$ .Figure 11.  $S_2$  via  $\phi$ .Figure 12.  $S_2$  via  $\phi$ .

Figure 12 discusses the function of  $S_2$  on Concentrations  $\phi$ . Take note that Concentrations  $\phi$

decreases as  $S_2$  increases. The reason for this is that as  $S_2$  increases, the difference between the ambient and surface concentrations  $\phi$  decreases, causing concentrations  $\phi$  to decay. The properties of  $Sc$  on concentrations  $\phi$  are displayed in Figure 13. For larger  $Sc$ , concentrations  $\phi$  here decrease. Actually, there is a lesser Brownian diffusion coefficient for bigger  $Sc$ , which has caused concentrations  $\phi$  decreases. The effect that  $\lambda$  has on concentrations  $\phi$  is shown in Figure 14. As  $\lambda$  is increased in this case, concentrations  $\phi$  and the thickness of the corresponding layer decreases. Furthermore, when  $\lambda > 0$  is compared to  $\lambda < 0$ , it is seen that the behavior is quite opposite. The behavior of  $n$  on concentrations  $\phi$  is depicted in Figure 15. It is evident that temperature  $\theta$  rises as  $n$  increases. Figure 16 displays the characteristics of  $K$  and  $\delta$  on skin friction. Higher  $K$  causes skin friction to rise whereas greater  $\delta$  causes it to decrease. The behaviors of  $Sc$  and  $\lambda$  on Sherwood number are discussed in Figure 17. There is no doubt that Sherwood's number rises as  $Sc$  and  $\lambda$  increase. Table 1 demonstrates the convergence of the series solutions. It is evident that, for temperature, concentration, and velocity, respectively, the convergence starts at the 30th order of approximations. The stability analysis for the solutions is depicted in the Figure 2.

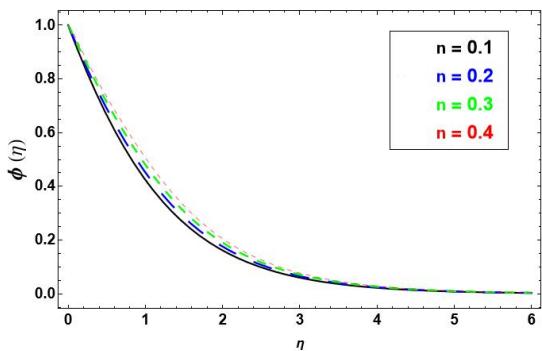


Figure 15.  $n$  via  $\phi$ .

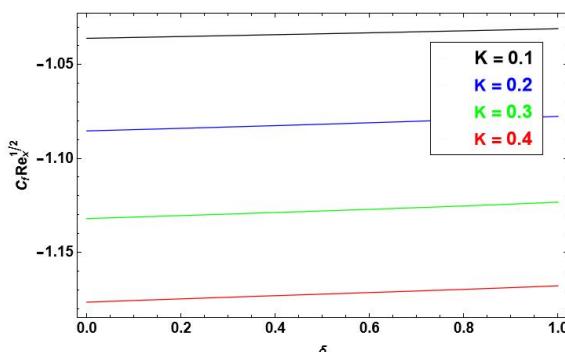


Figure 16. Skin Friction on  $K$  and  $\delta$ .

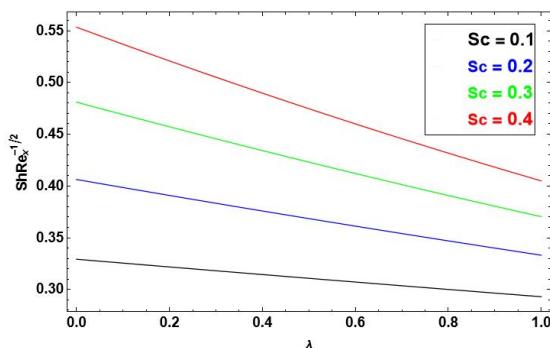


Figure 17. Sherwood on  $Sc$  via  $\lambda$ .

## 7 Conclusions

The following important points are included in the summary of this article's conclusion:

- For increasing  $n$ , there is an increase in temperature  $\theta$ , concentration  $\phi$ , and velocity  $f'$ .
- As  $K$  increases, the viscosity decreases, increasing the thickness of the momentum and velocity layers.
- Non-Fourier's heat flux has a temperature that is lower than Fourier's approach.
- Greater  $\alpha$  results in increased velocity and thickness of the momentum layer.

**Table 1.** The Homotopic solutions for convergence when  $n = \delta = S_1 = 0.6$ ,  $K = \epsilon_1 = \lambda = q = 0.4$ ,  $S_2 = \gamma = \alpha = 0.1$ ,  $Sc = 0.8$  and  $Pr = 0.9$ .

| Approximation Order | $-f''(0)$ | $-\theta'(0)$ | $-\phi'(0)$ |
|---------------------|-----------|---------------|-------------|
| 1                   | 0.8219    | 0.8554        | 0.7712      |
| 5                   | 0.8346    | 1.0318        | 0.6555      |
| 10                  | 0.8381    | 1.0646        | 0.5145      |
| 15                  | 0.8394    | 1.0655        | 0.5073      |
| 20                  | 0.8401    | 1.0775        | 0.5087      |
| 25                  | 0.8401    | 1.0835        | 0.5129      |
| 30                  | 0.8401    | 1.1563        | 0.5236      |
| 35                  | 0.8401    | 1.1563        | 0.5236      |
| 40                  | 0.8401    | 1.1563        | 0.5236      |

- When  $\epsilon_1$  increases, temperature decreases when  $Pr$  and  $\chi$  increase.
- Temperature  $\theta$  and concentrations  $\phi$  decreases as  $S_1$  and  $S_2$  increases.

## Data Availability Statement

Data will be made available on request.

## Funding

This work was supported without any funding.

## Conflicts of Interest

The authors declare no conflicts of interest.

## Ethical Approval and Consent to Participate

Not applicable.

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